

Discrete Element Modeling

Part 3. Two Phase Flow

Bruno Chareyre

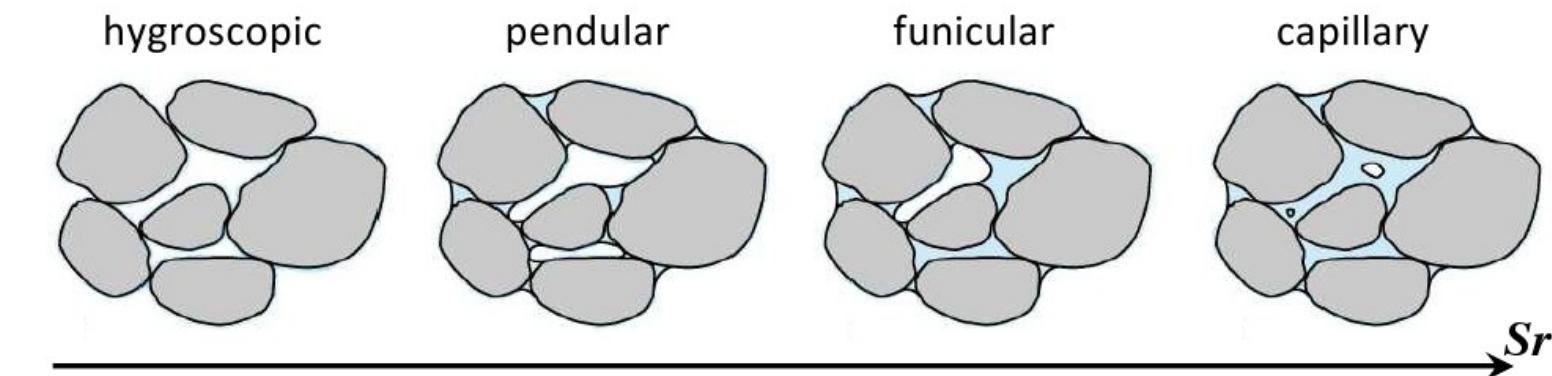
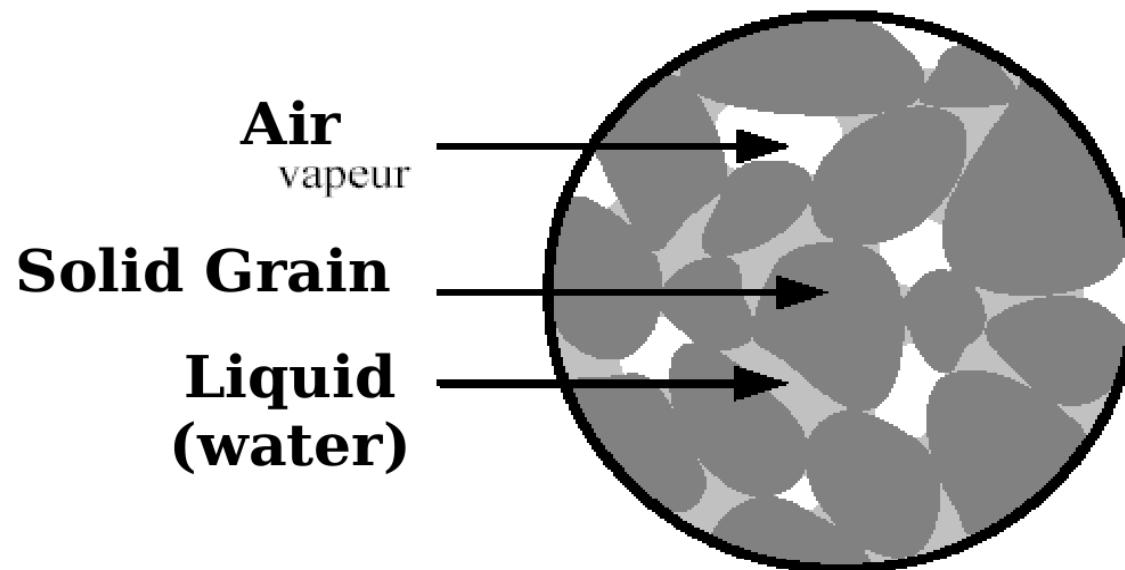




Part 3. Two Phase Flow

- macro-continuum scale
- micro-continuum scale
- pore scale

Capillarity



Macro-scale modeling

Unknowns:

air pressure p_n ,

water pressure p_w ,

water content S_r (“sat. degree”)

Equations:

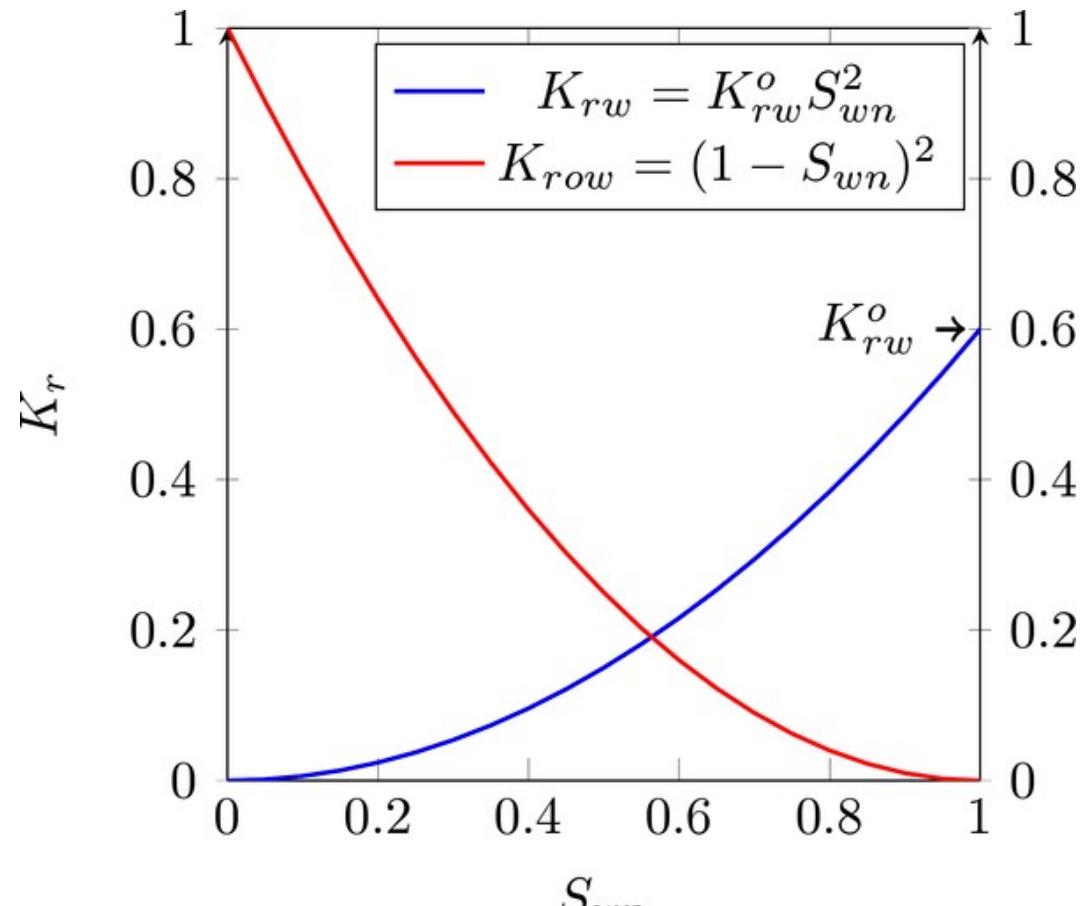
$$\operatorname{div}(v_w - v_s) + dS_r/dt = 0 \quad (\text{mass balance})$$

$$p_c = p_n - p_w = p_c(S_r) \quad (\text{water retention})$$

$$K = K(S_r) \quad (\text{Darcy with partial perm.})$$

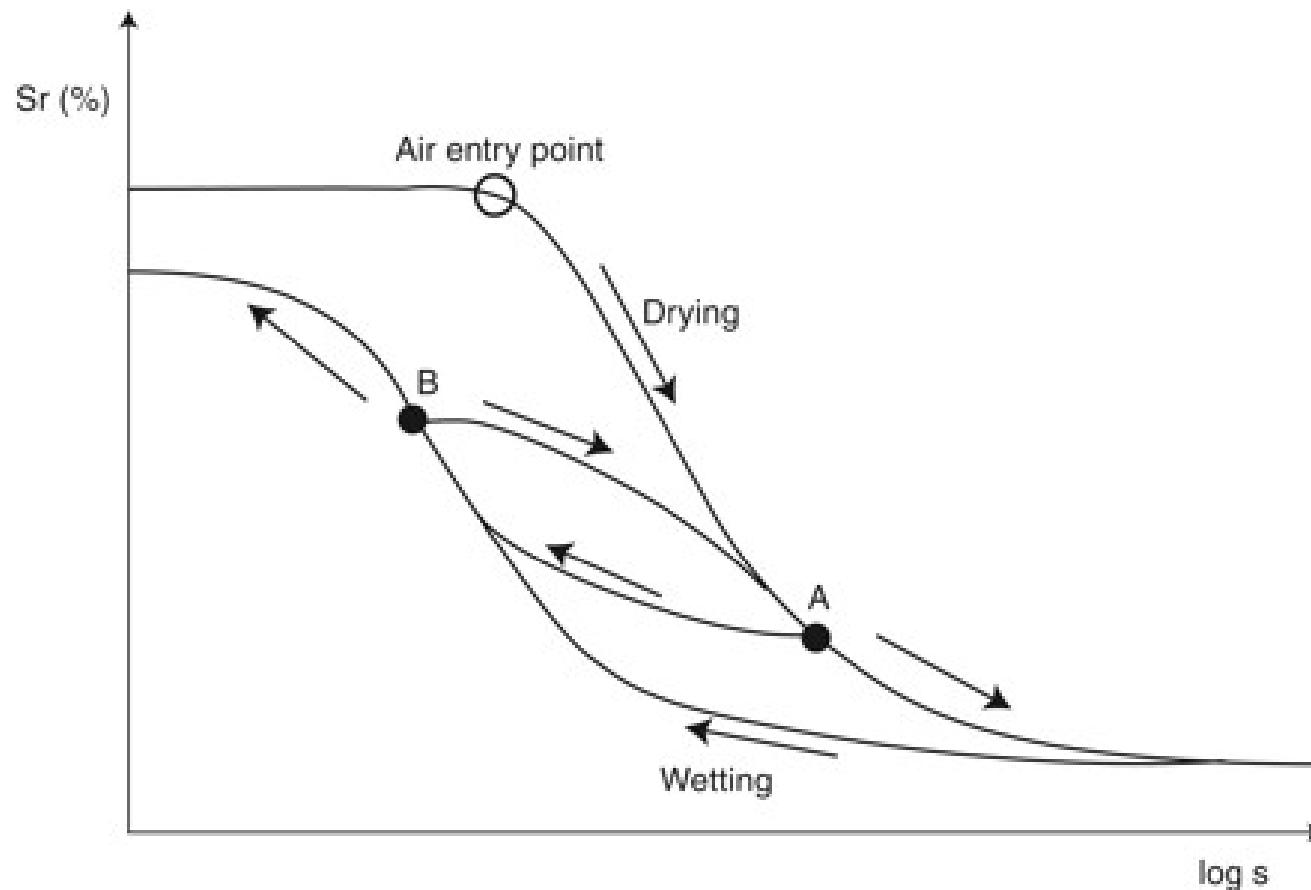
$$\sigma' = \sigma - S_r p_c \mathbf{I} \quad (\text{Bishop's effective stress})$$

Macro-scale modeling



Relative permeability, Brooks & Corey (1964)

Macro-scale modeling



Relative permeability, Brooks & Corey (1964)

Micro-scale modeling

Unknowns:

air pressure p_n ,

water pressure p_w ,

geometry of phases and interfaces

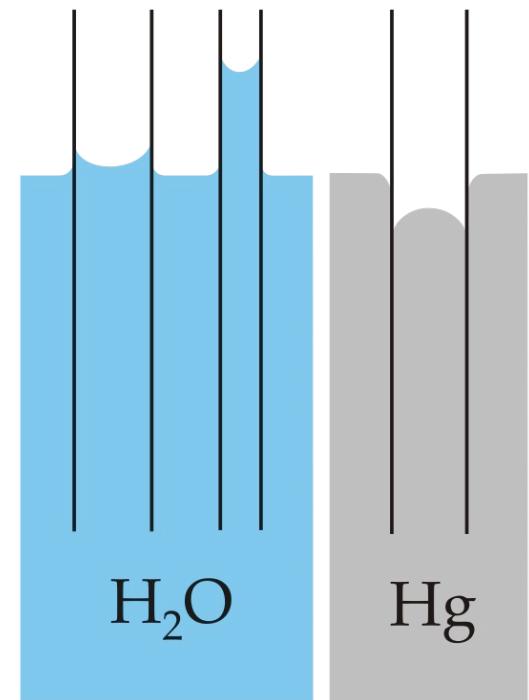
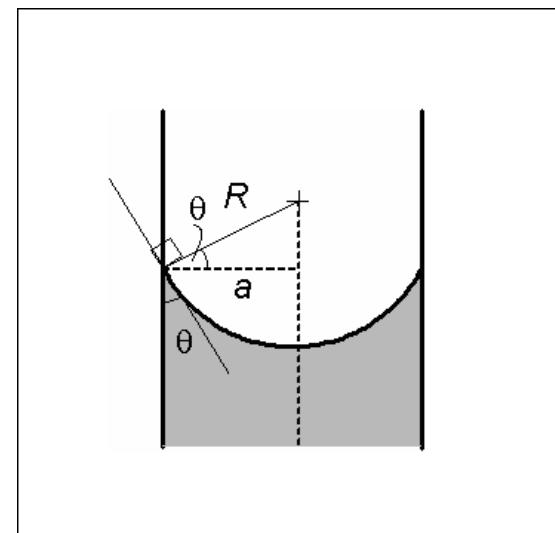
Equations:

Young-Laplace

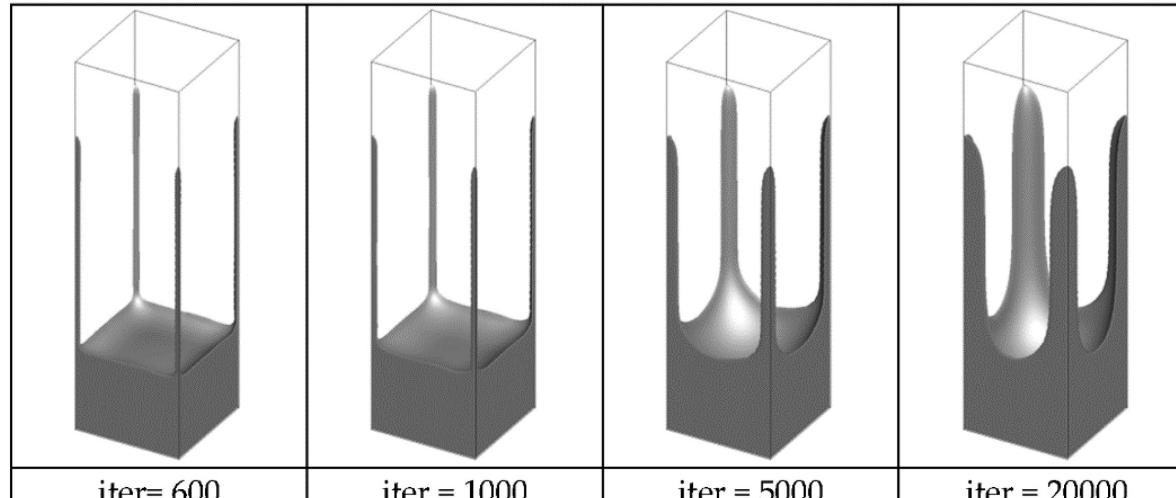
$$\begin{aligned}\Delta p &= -\gamma \nabla \cdot \hat{n} \\ &= 2\gamma H \\ &= \gamma \left(\frac{1}{R_1} + \frac{1}{R_2} \right)\end{aligned}$$

Jurin's law

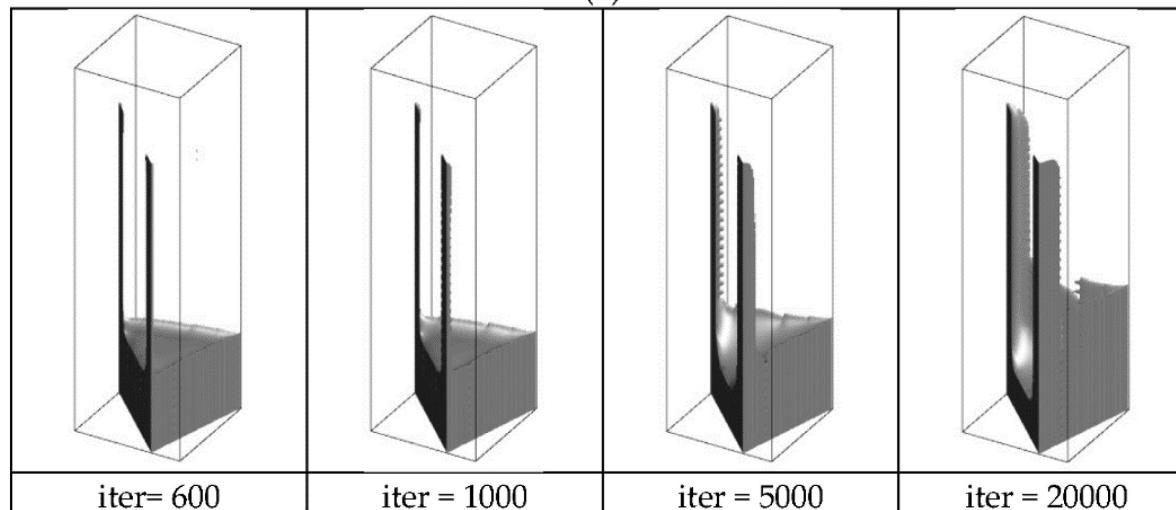
$$h = \frac{2\gamma \cos \theta}{r\rho g}$$



Micro-scale modeling



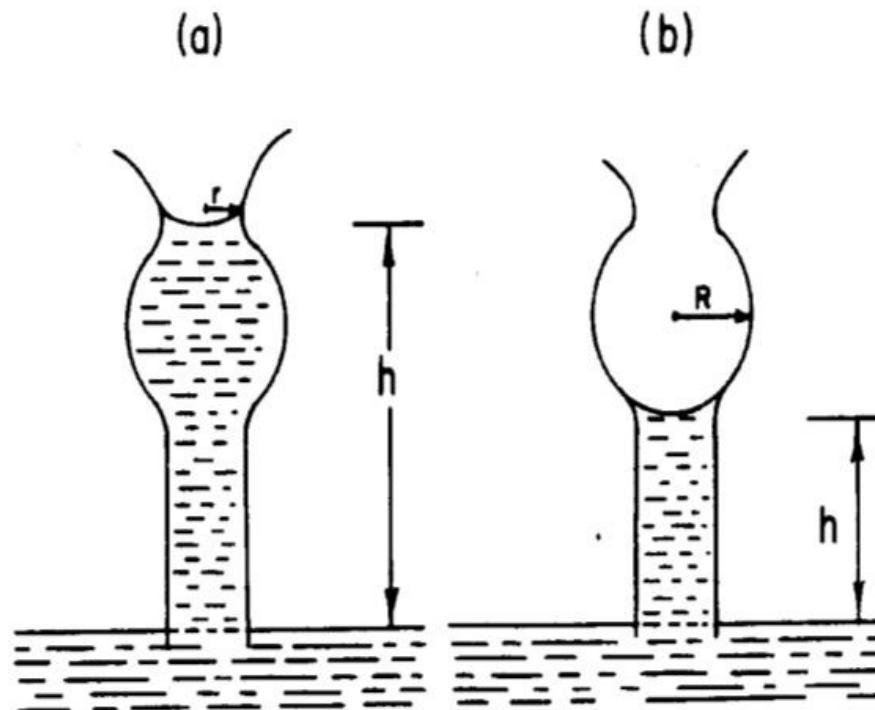
(a)



(b)

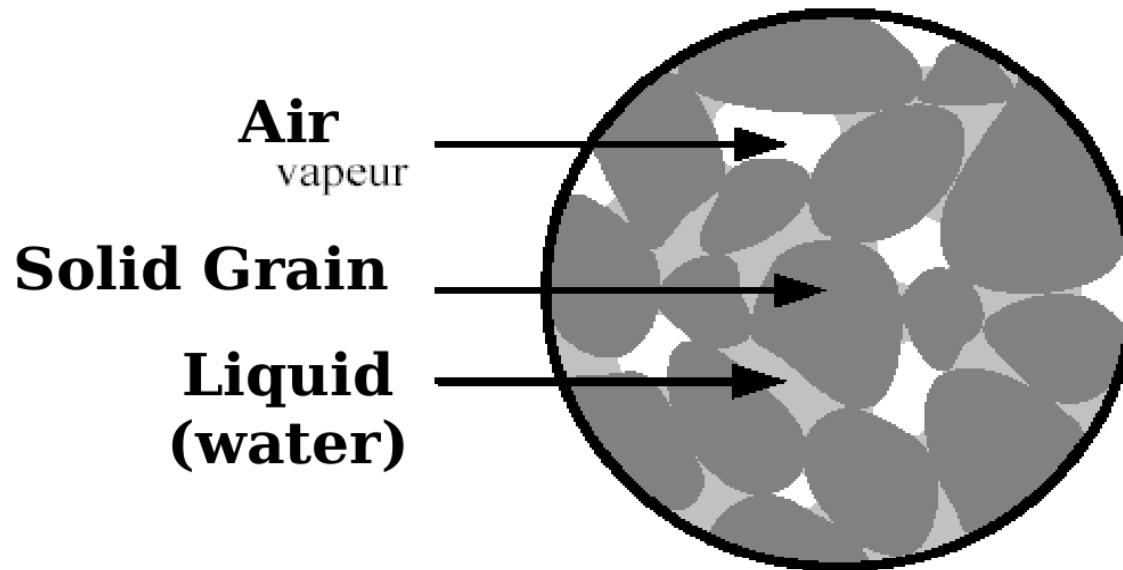
Micro-scale modeling

Hysteresis



"Ink-bottle" effect determines equilibrium height of water in a variable-width pore :
(a) in capillary drainage (desorption) and
(b) in capillary rise (sorption).

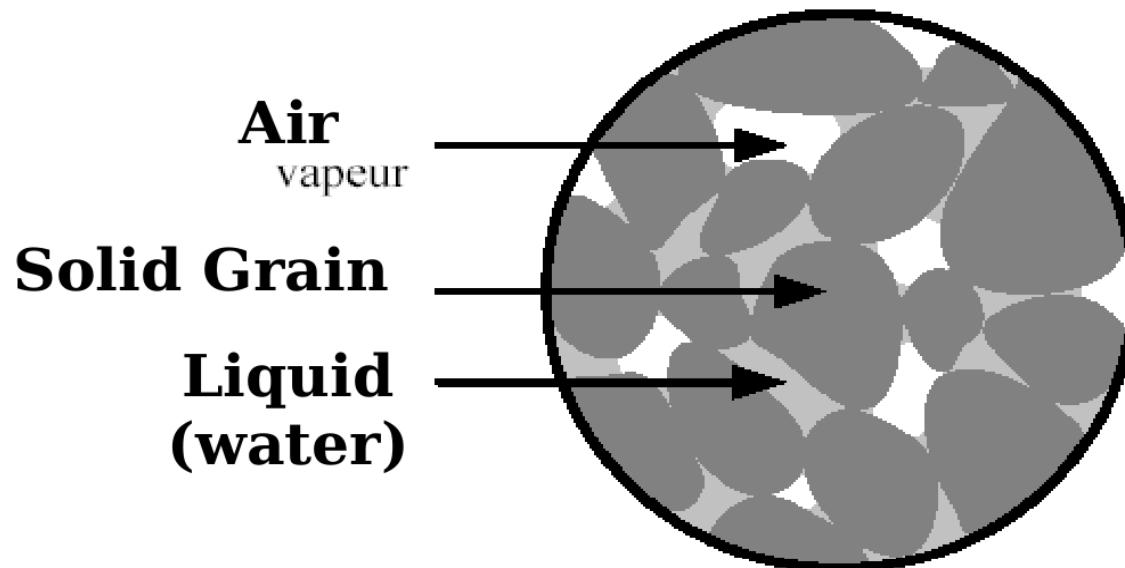
Micro-scale modeling



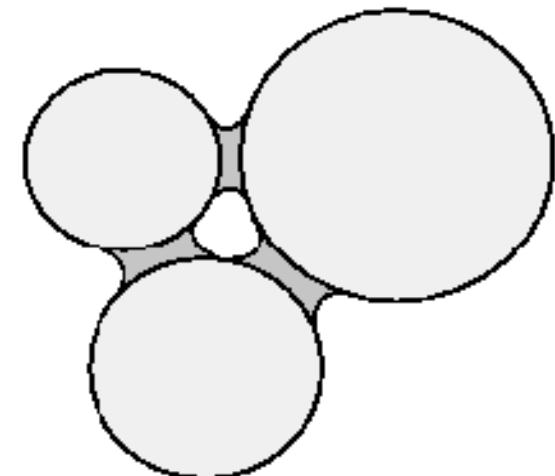
Fluid flow in such system goes through various processes:

- 1-phase flow in saturated subdomains
- film flow at the surface of the solid phase or “corner” flow
- movement of interfaces (e.g. moving bubbles or change of S_r)
- vapor transfer

Micro-scale modeling



At **low water content** levels
interfacial phenomena lead to
intergranular water menisci

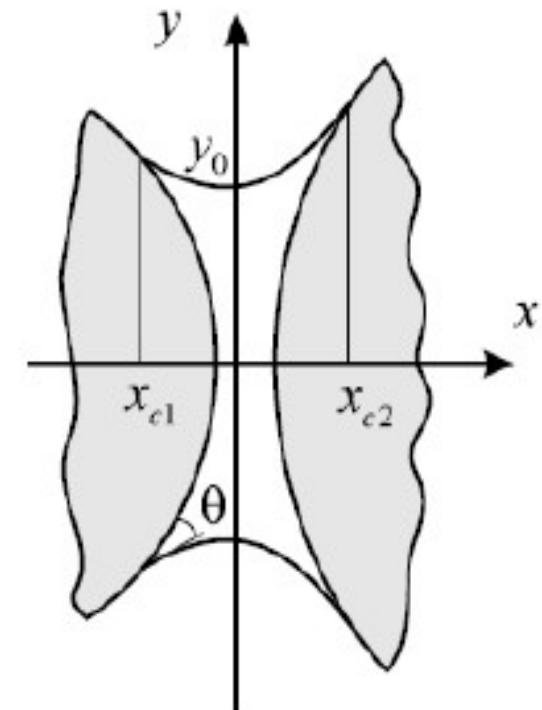
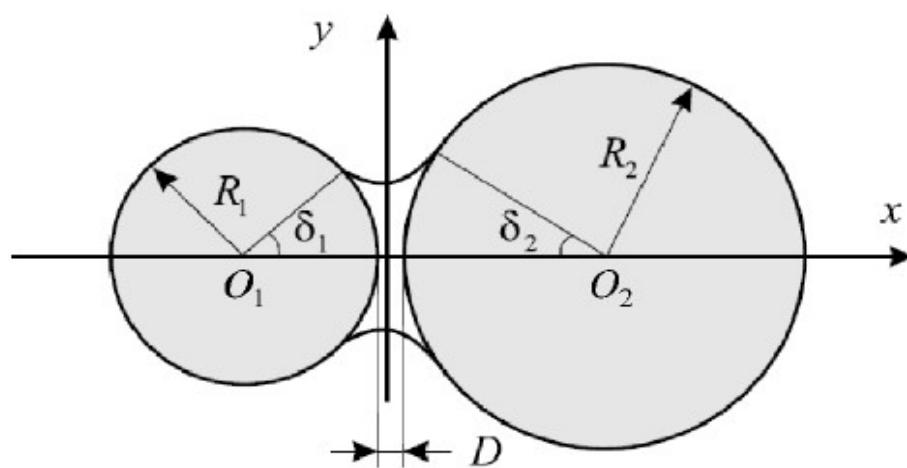


Micro-scale modeling: pendular bridge

Young-Laplace equation:

$$p_c = \gamma_{wn} C$$

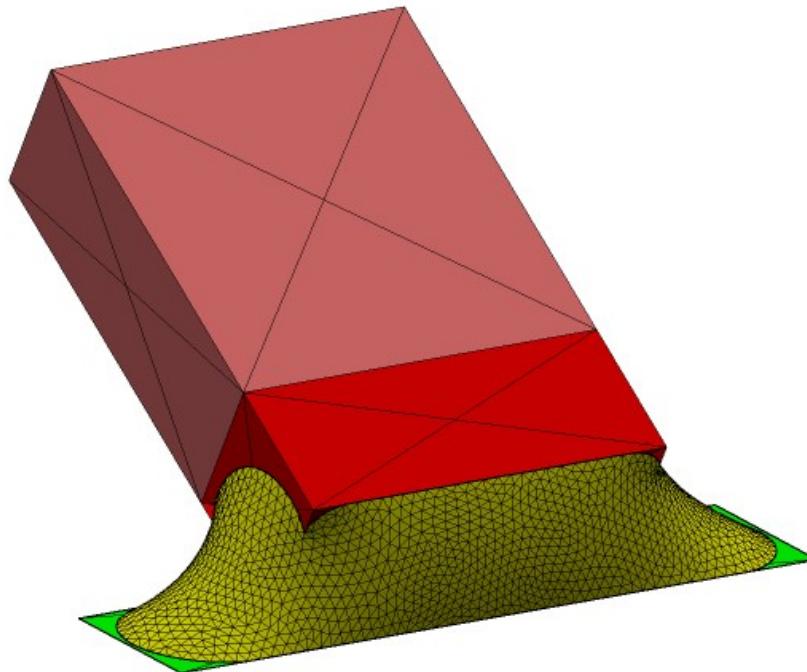
$$C^* = \frac{-1}{y^* \sqrt{1 + y'^{*2}}} + \frac{y''^*}{(1 + y'^{*2})^{\frac{3}{2}}}$$



$$\left\{ \begin{array}{l} F_{cap} = 2\pi\sigma y_0 + \pi\Delta u y_0^2 \\ V_{cap} = \pi \int y^2(x).dx \end{array} \right.$$

Micro-scale modeling: numerical methods

Minimization techniques

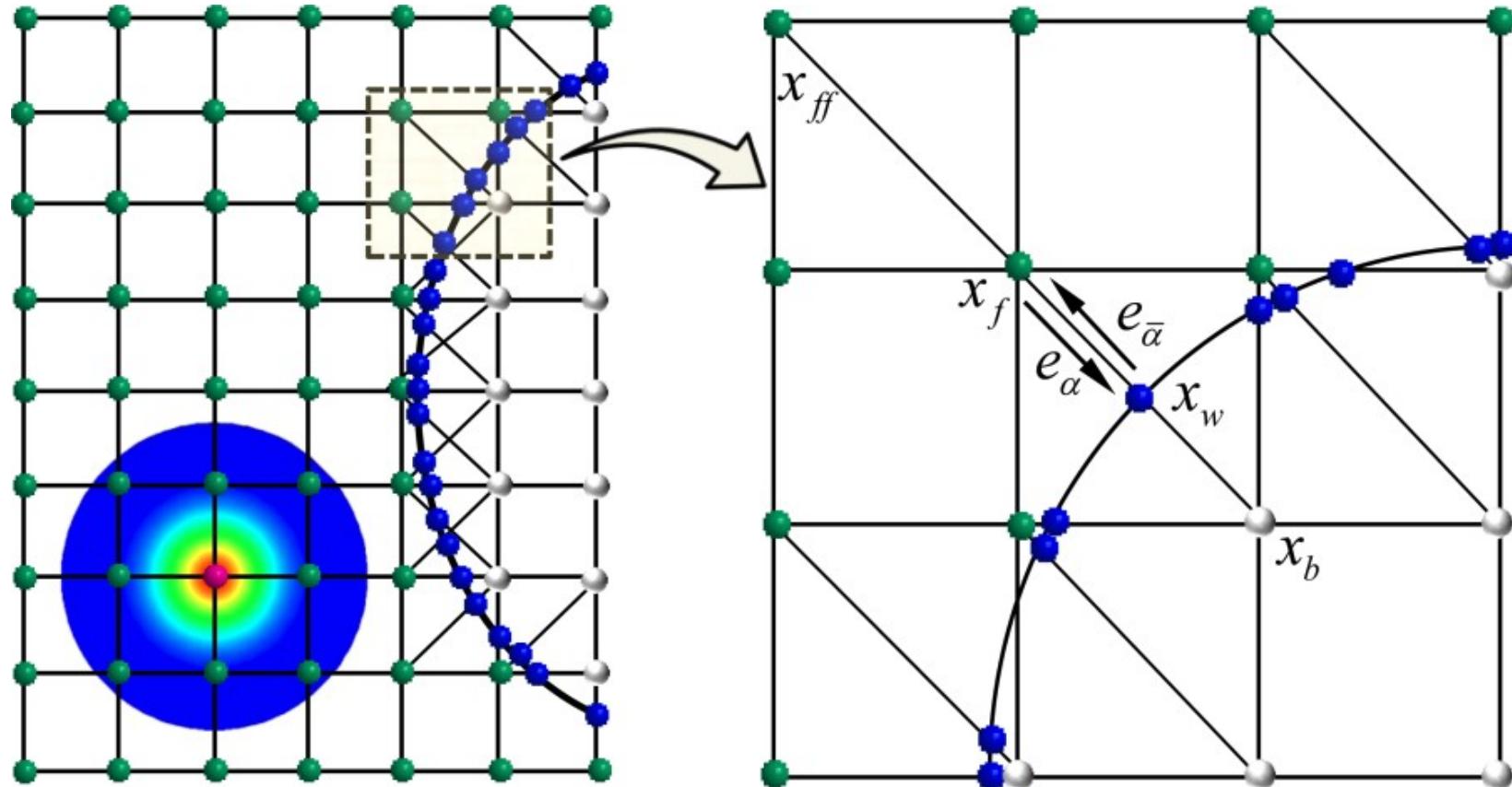


Surface Evolver

<http://facstaff.susqu.edu/brakke/evolver/evolver.html>

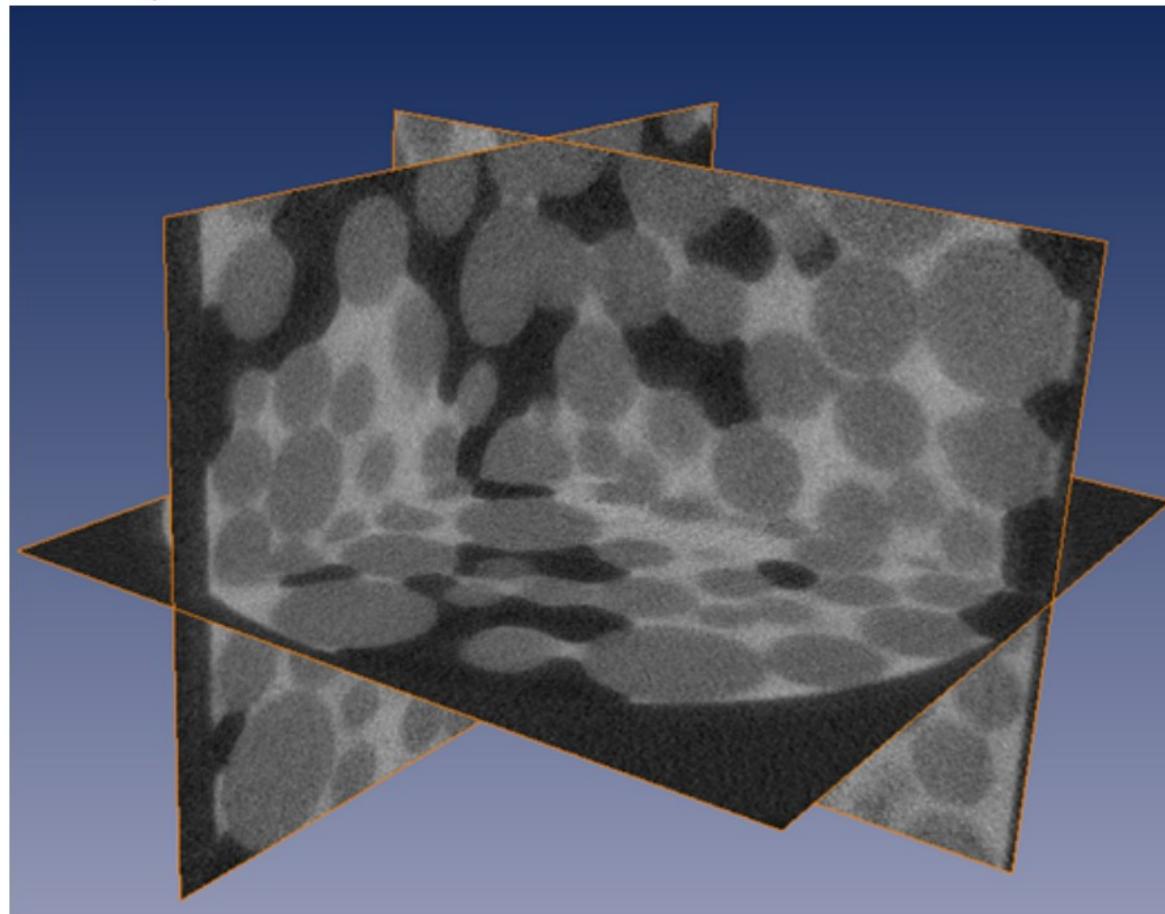
Micro-scale modeling: numerical methods

Lattice-Boltzmann method, Shan & Chen 2-phase field
(and live examples)



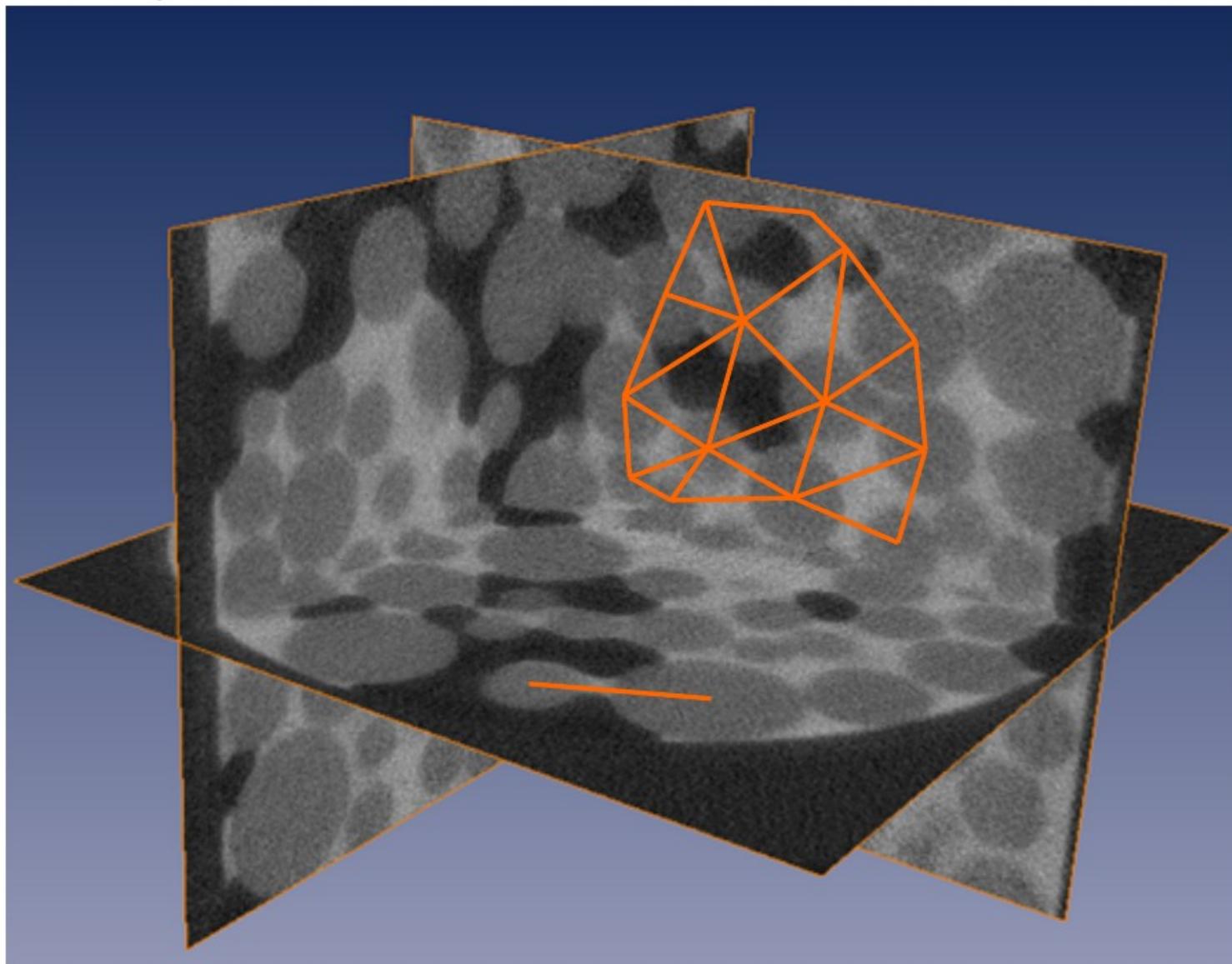
Pore-scale modeling

Distribution of immiscible phases in *quasistatic* primary drainage
(Culligan et al.¹)

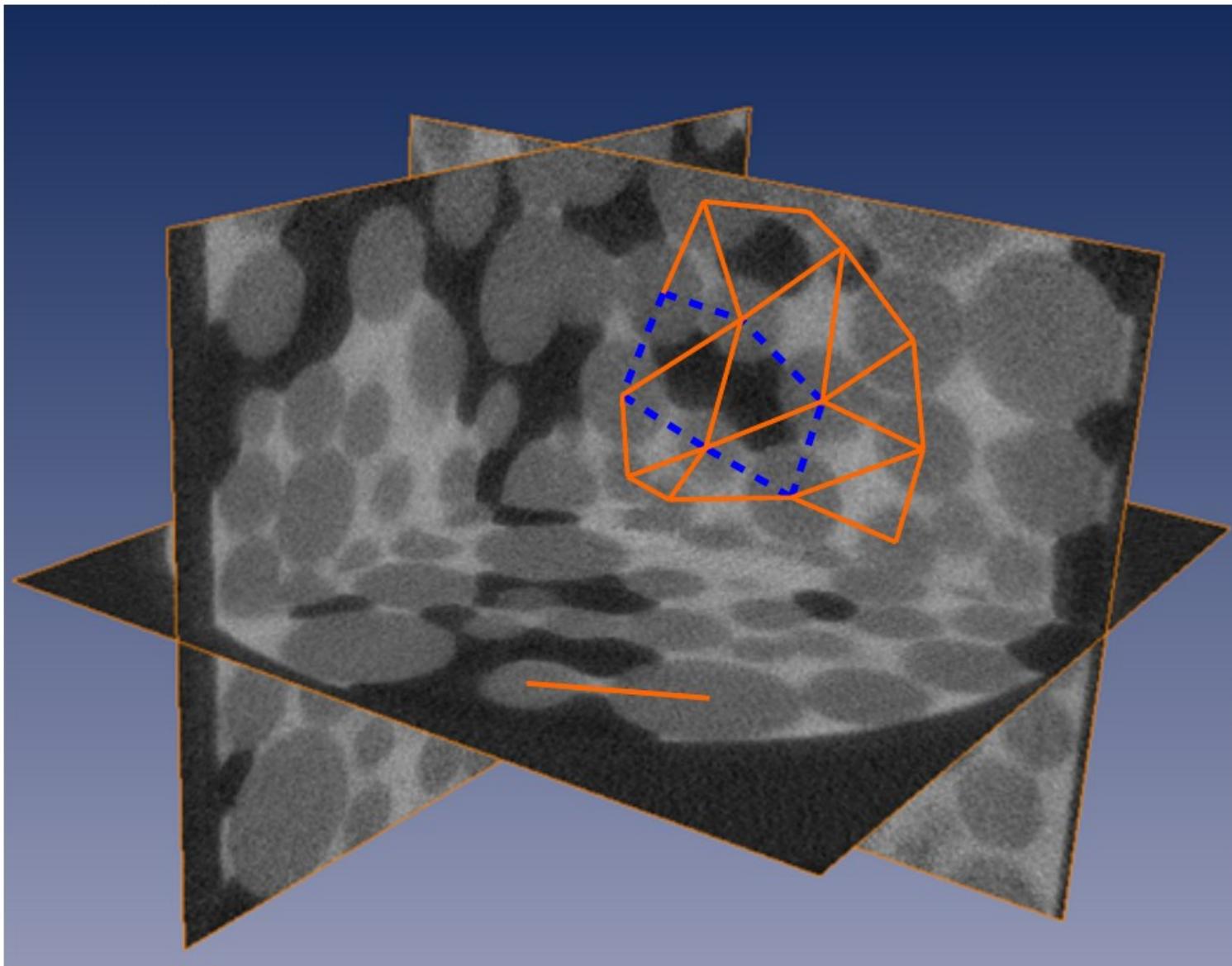


¹Culligan, Wildenschild, Christensen et al., *Water Resources Res.* (2004)

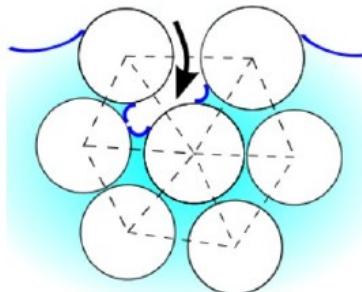
Pore-scale modeling



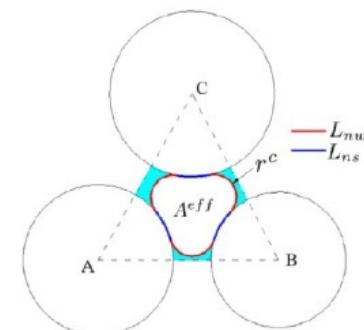
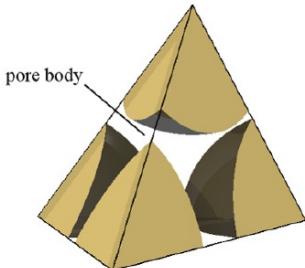
Pore-scale modeling



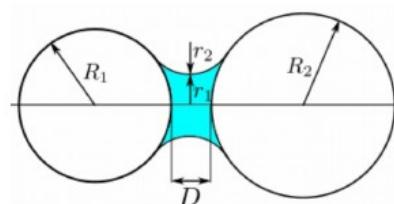
Pore-scale modeling



Pores: binary transition between saturated and dry states



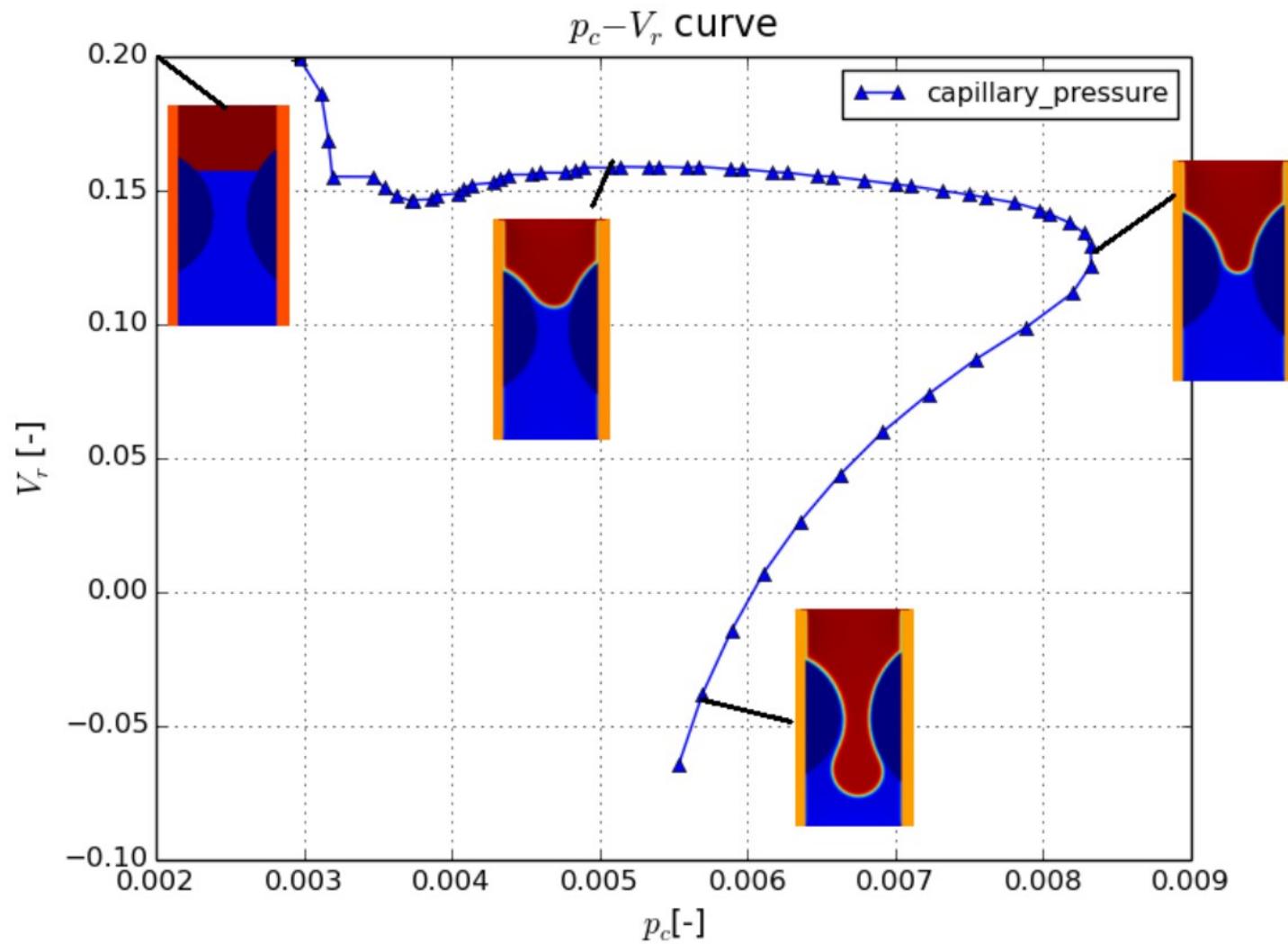
Throats: local rule $p_c < p_c^e$ + parametrization of p_c^e wrt. local geometry (MSP method)
(p_c^e : local entry capillary pressure)



Pendular bridge

Pore-scale modeling

The 3-sphere problem

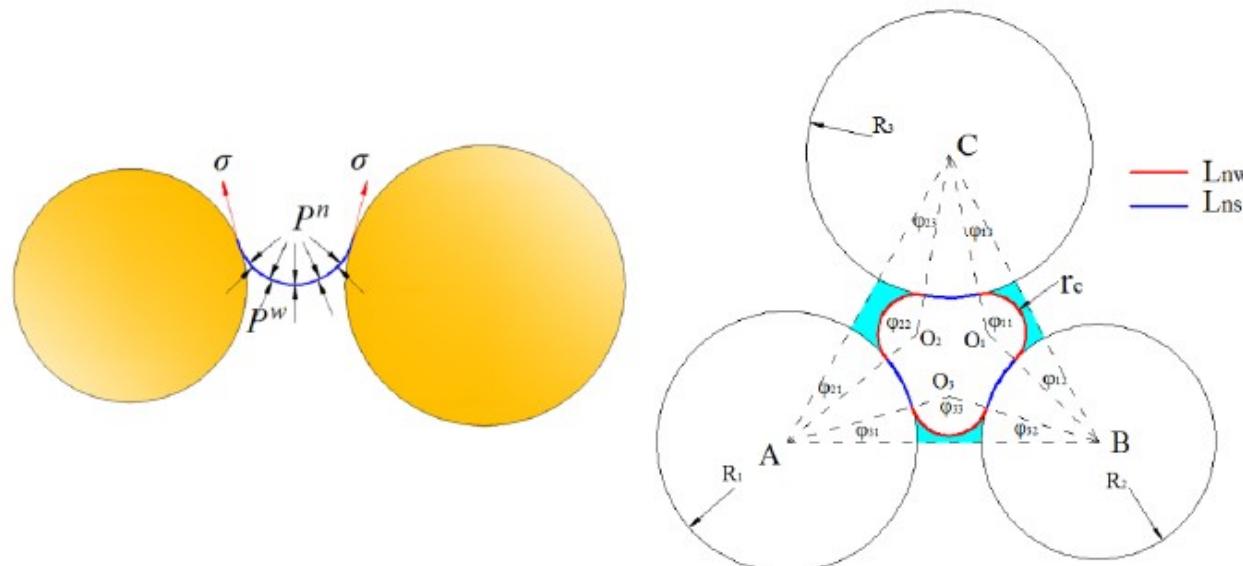


Pore-scale modeling

The 3-sphere problem

The approach for calculating P_e^c is based on MS-P method suggested by Ma et al. (1996); Mayer and Stowe (1965); Princen (1969) and Joekar-Niasar et al. (2010), which follows from the balance of forces for pore throat section.

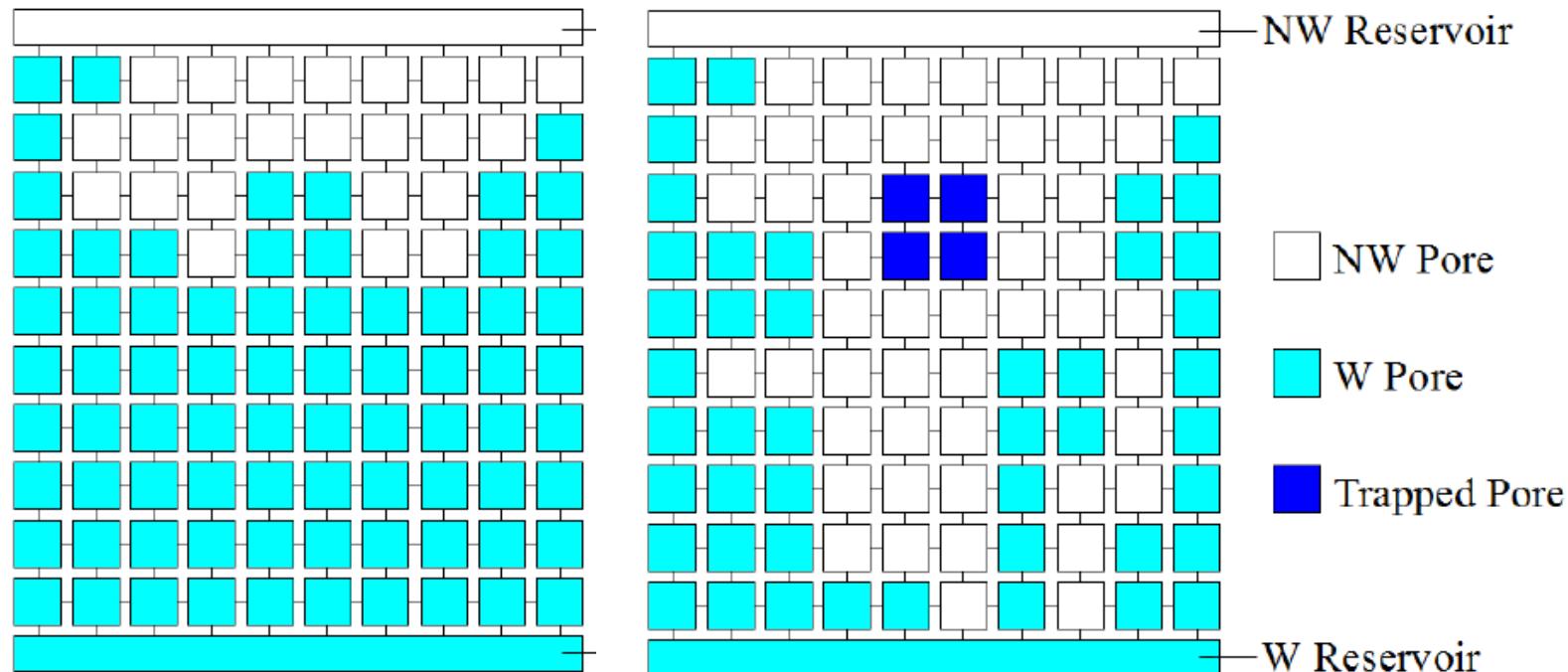
$$\sum F(r_c) = F^c(r_c) + T^I(r_c) = 0$$



Pore-scale modeling

Network evolution and disconnected phases

An idealized view of primary drainage



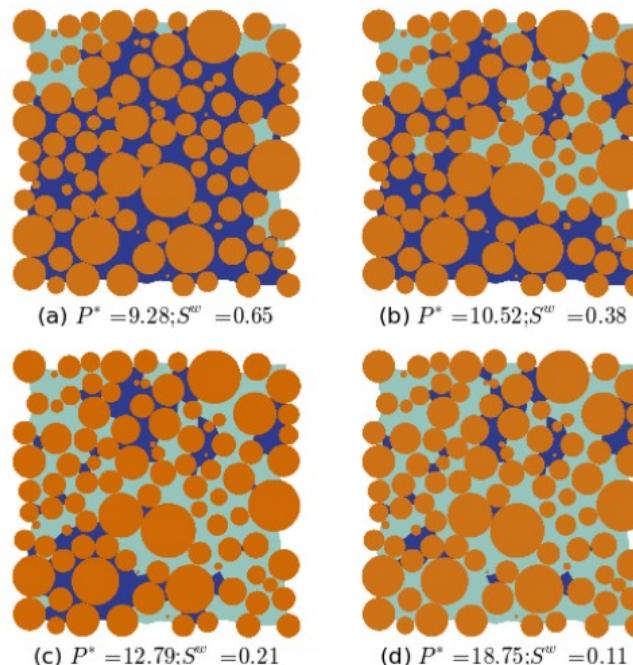
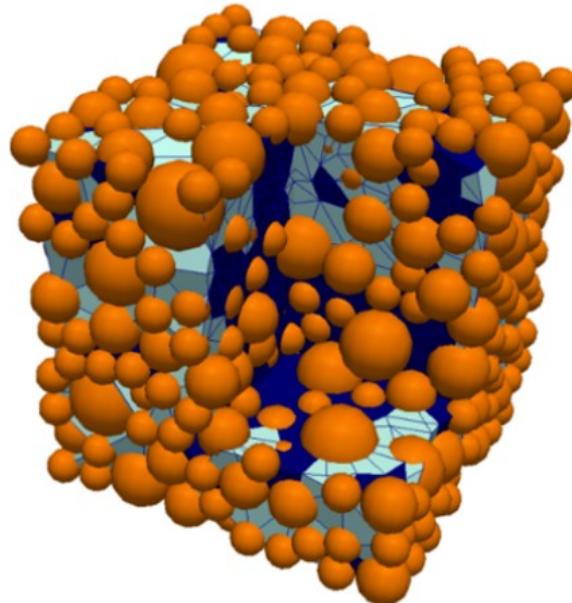
Pore-scale modeling

Network evolution and disconnected phases

The network model has been implemented in C++, and it is freely available as an optional package of the open-source software **Yade** (Smilauer et al. (2010)).

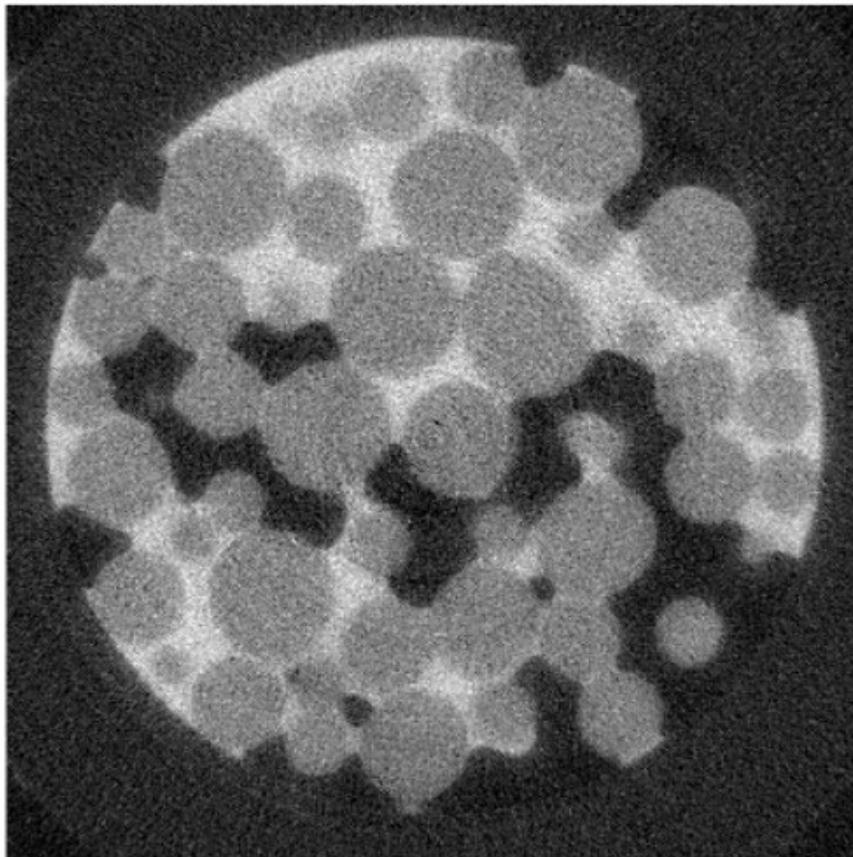
The C++ library CGAL (Boissonnat et al. (2002)) is used for the triangulation procedure.

S^R

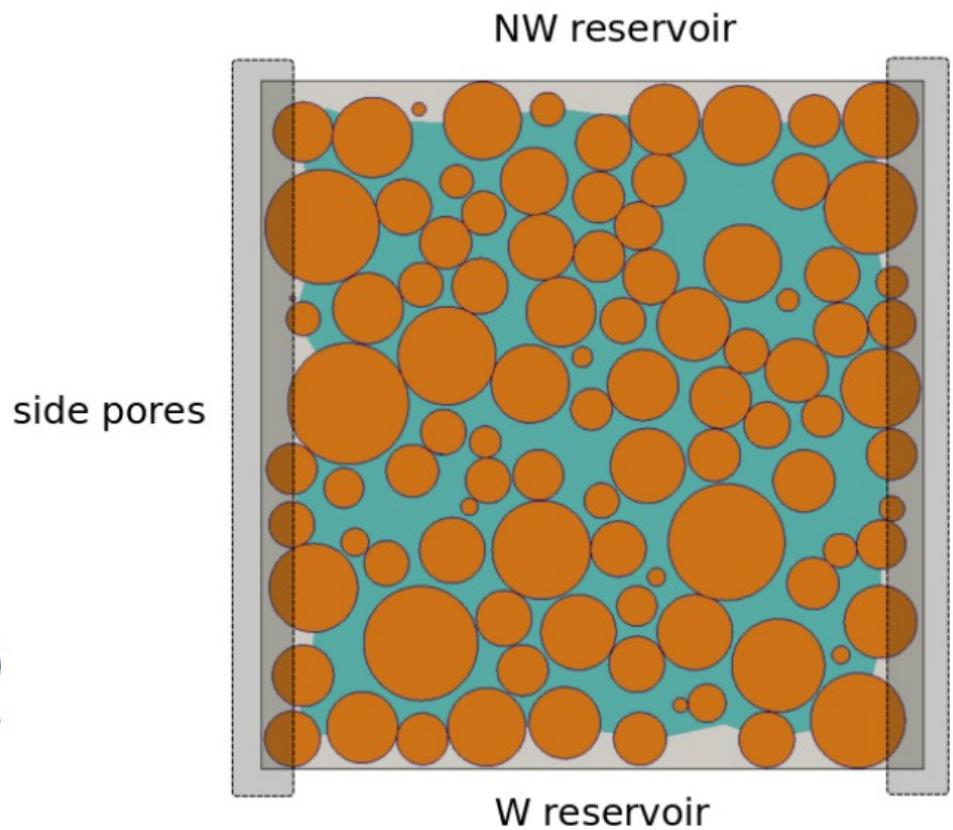


Pore-scale modeling

Model verification



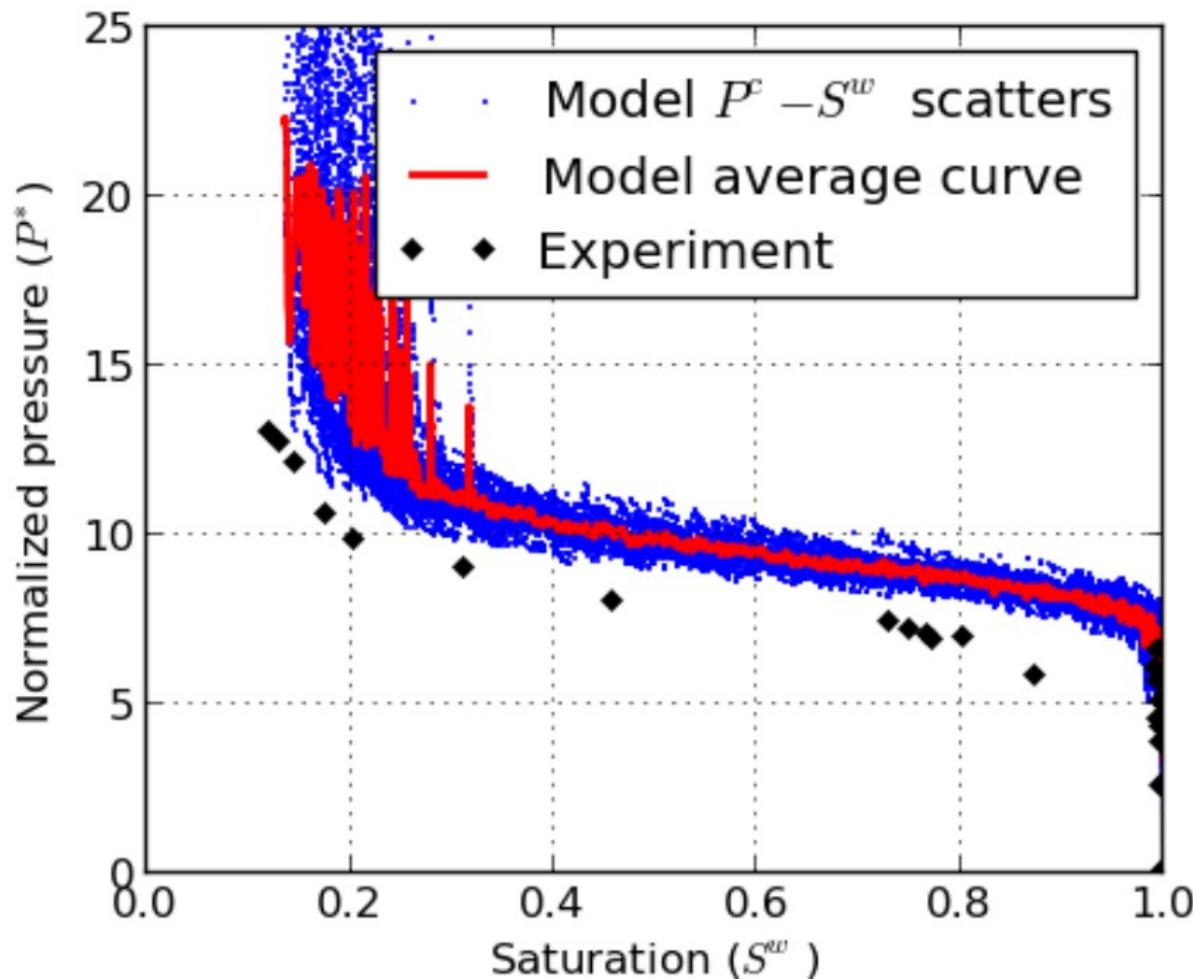
R



Culligan K. et al., 2004

Pore-scale modeling

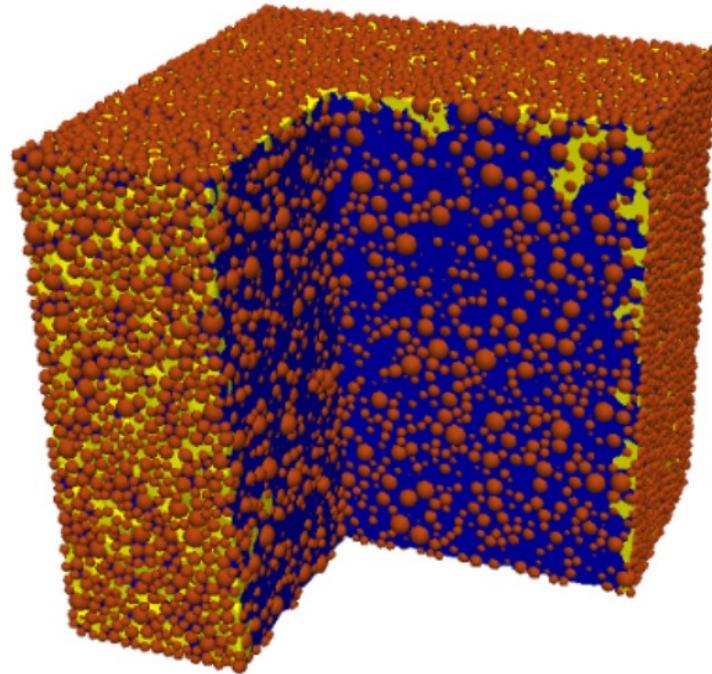
Model verification



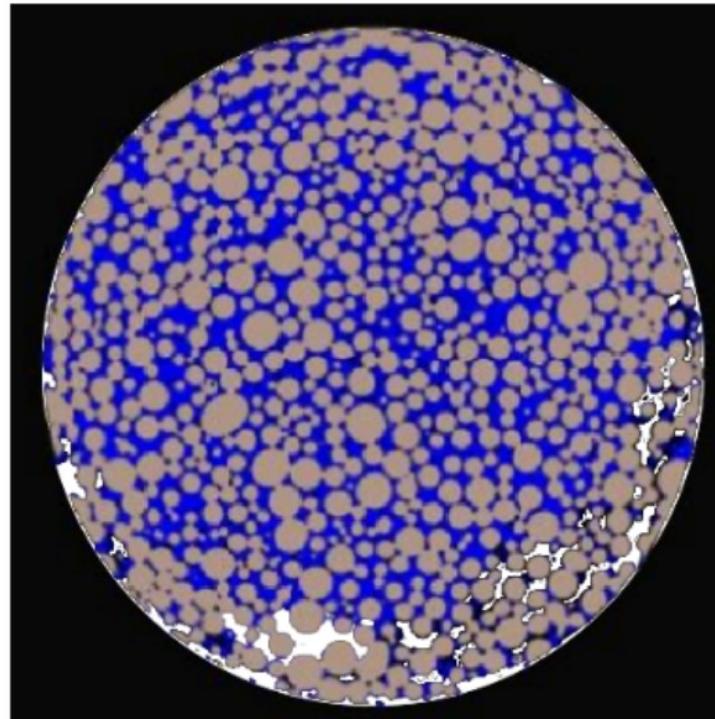
Pore-scale modeling

Model verification

Permeable side boundary condition (open side). Experimental scan image by Khaddour G. et al. (2012).



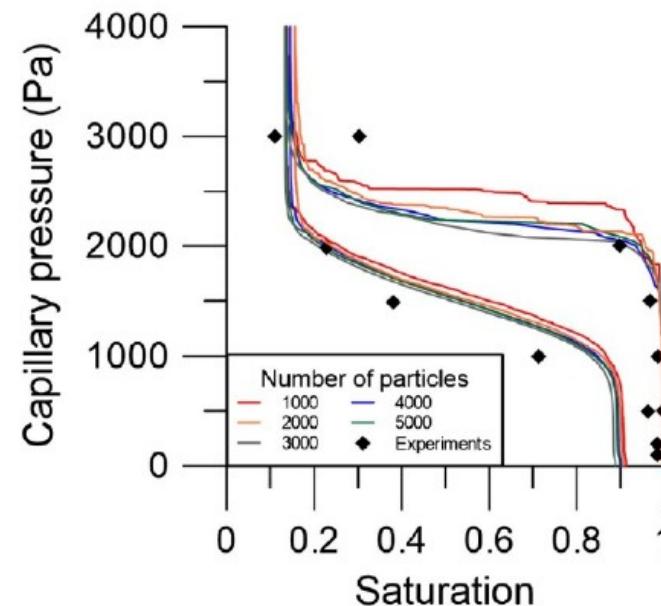
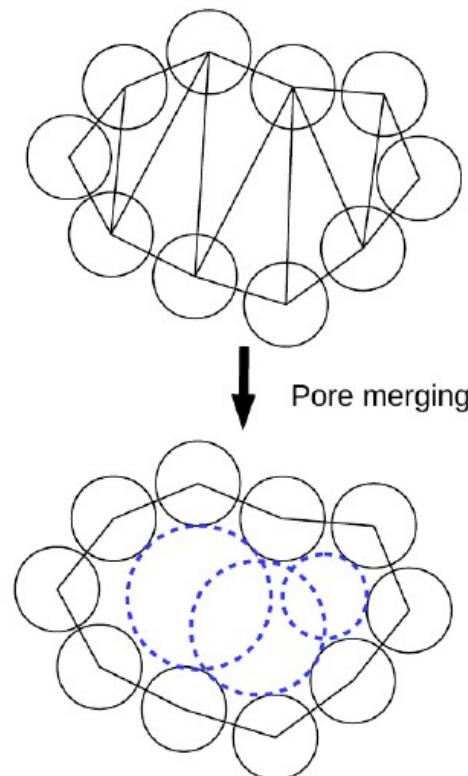
(a)



(b)

Pore-scale modeling

The imbibition process is mainly controlled by the pore size instead of the throat size. A pore-merging algorithm has been developped¹



¹Sweijen, Nikooee, Hassanizadeh, Chareyre, *Transp. Porous Med.* 2016

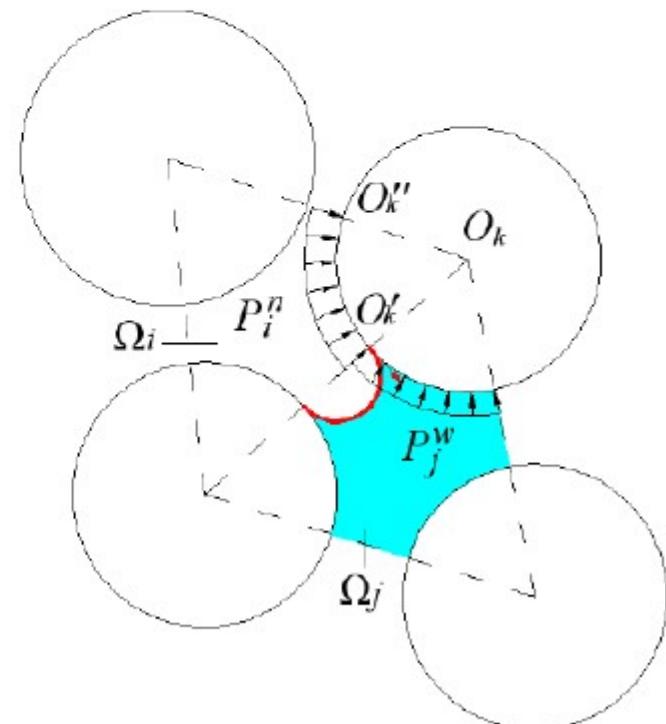
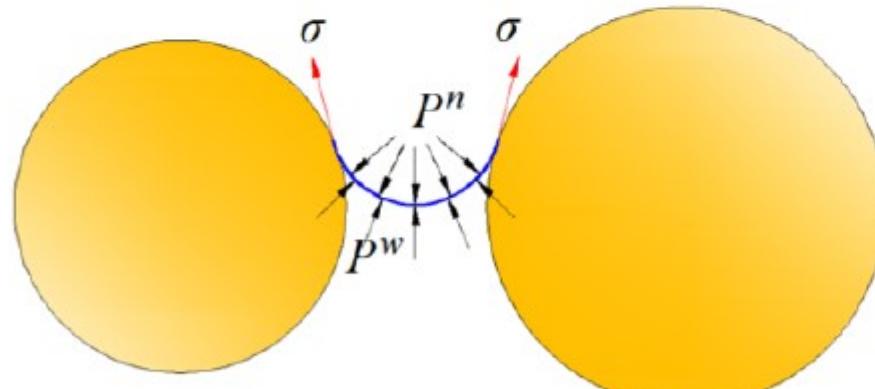


Pore-scale modeling

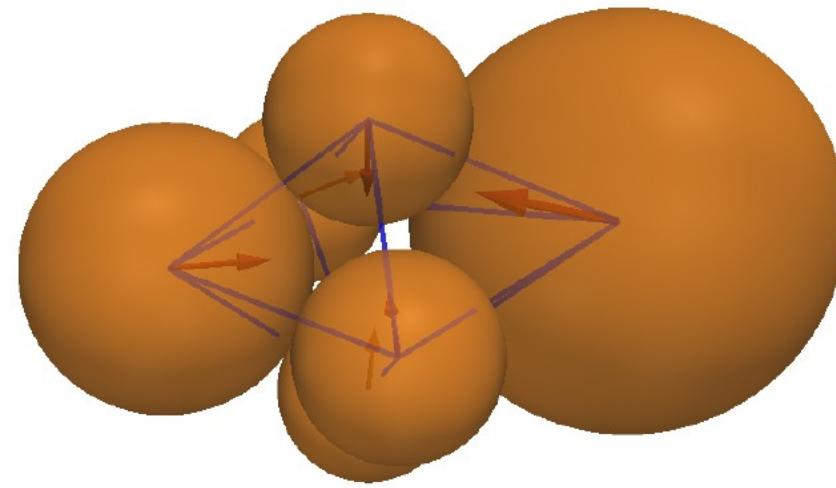
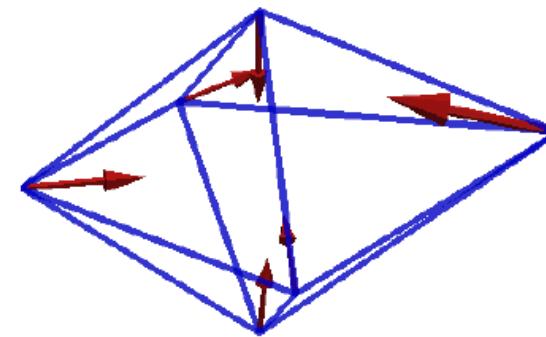
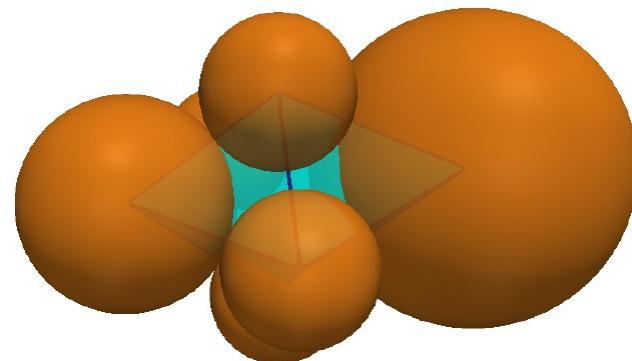
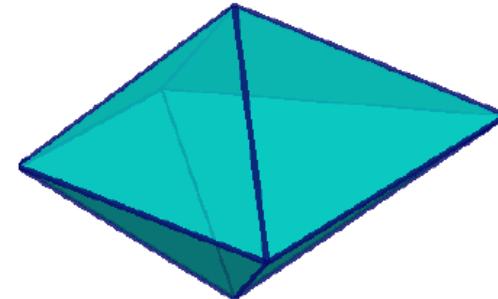
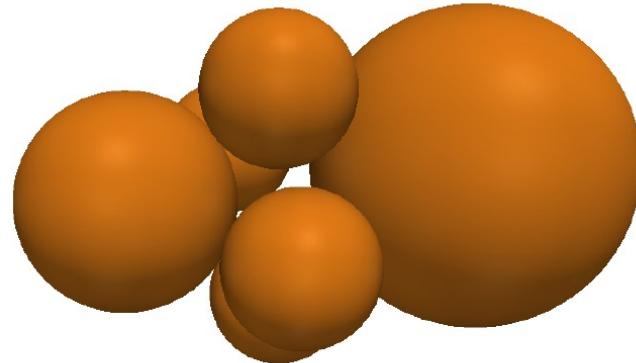
Capillary force and deformation

The total force F^k generated on particle k includes the effects of W-phase P^w , NW-phase P^n and NW-W interface tension σ^{nw} .

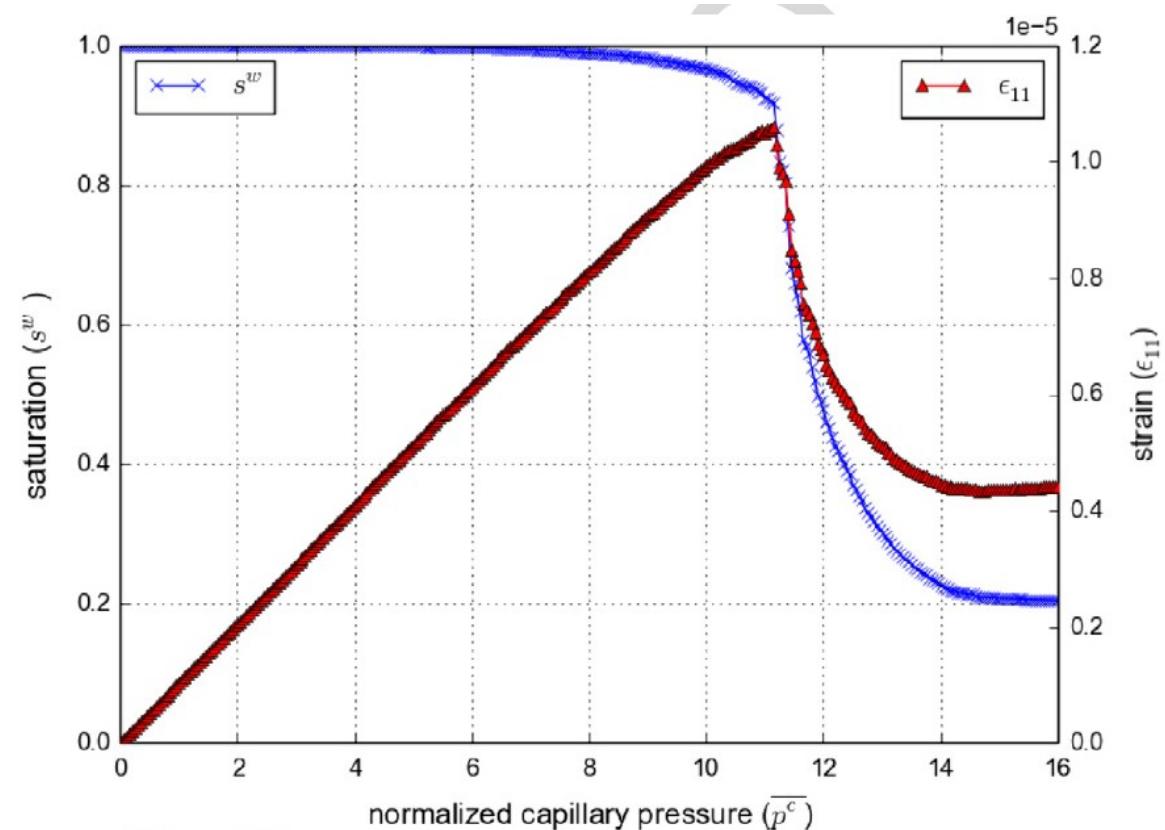
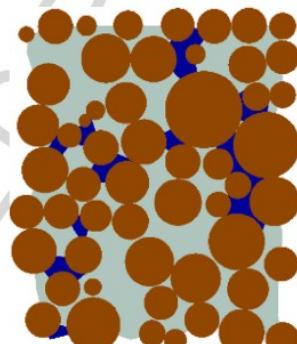
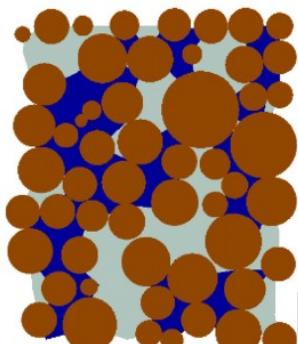
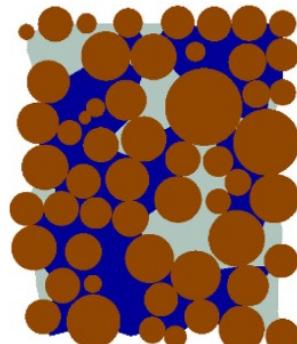
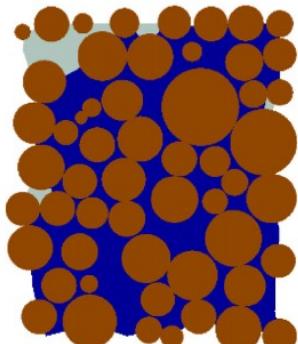
$$F^k = F^{n,k} + F^{w,k} + F^{\sigma,k}$$



Pore-scale modeling



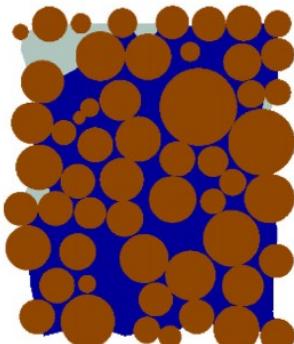
Pore-scale modeling



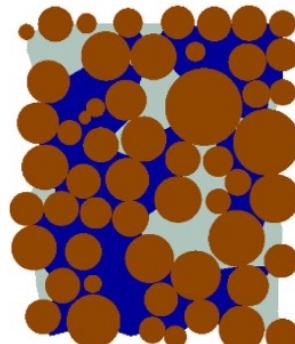
Pore-scale modeling

Conclusion:

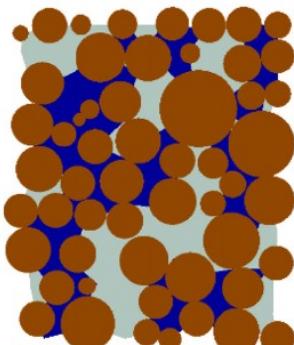
The optimal water content for a sand castle is $S_r=1$ (?!!...)



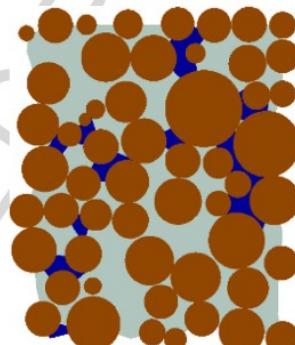
(a) $\bar{p}^c = 7.25; s^w = 0.96$.



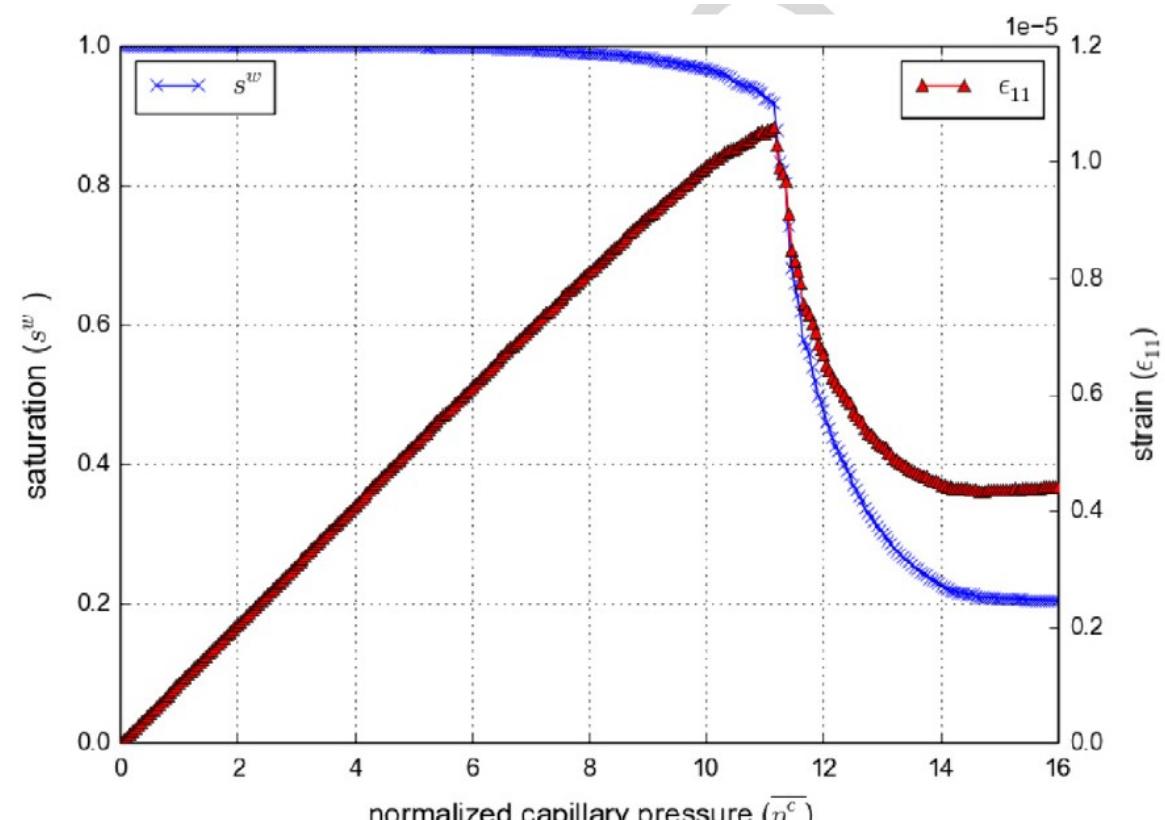
(b) $\bar{p}^c = 8.85; s^w = 0.68$.



(c) $\bar{p}^c = 9.00; s^w = 0.62$.

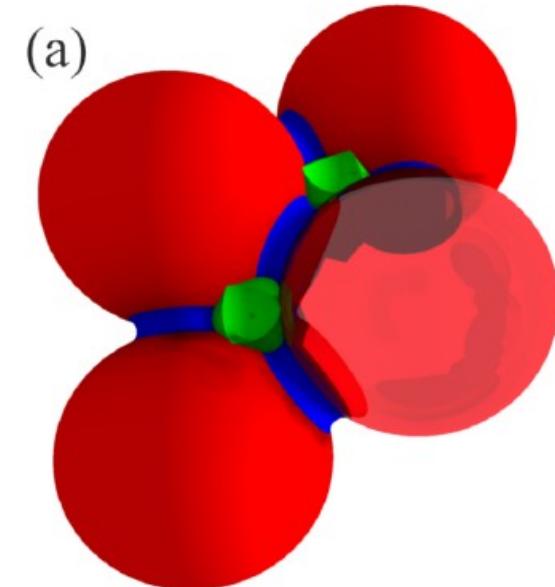


(d) $\bar{p}^c = 13.2; s^w = 0.18$.



- Imbibition (still), cooperative invasion at macro-throats
- Large deformations, splitting or merging trapped clusters or bridges (Melnikov et al.¹)
- Residual permeability in the drained regions (Mani et al.²), i.e. film flow and/or vapor transfer.
- Partial wettability.

On all aspects, a need for high resolution experiments and/or solutions by micro-continuum models.



¹Melnikov, Mani, Wittel, Thielmann, Herrmann, *PRE* 2015

²Mani, Kadau, Herrmann, *PRL* 2012